# Contribution to the Study of Methanol Oxidation on MoO3

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The oxidation of methanol on molybdenum trioxide (with its lattice oxygen only) was investigated. The composition of the gaseous phase analyzed by means of a mass spectrometer changed after the reduction of the oxygen surface layer. A change of the oxidation mechanism due to the lowering of the valency of Mo<sup>6+</sup> to Mo<sup>4+</sup> is suggested.

MoO<sub>3</sub> is contained in the Fe<sup>3+</sup>-Mo<sup>6+</sup>-O mixed catalysts which are widely used for the selective oxidation of methanol to formaldehyde (1-8). The mechanism of methanol oxidation on these mixed catalysts has not yet been quite explained; for that reason we have studied separately the behavior of both cations in the form of their oxides. The methanol oxidation on Fe<sub>2</sub>O<sub>3</sub> will be dealt with in another publication.

Oxidizing methanol on MoO<sub>3</sub> in the presence of oxygen in the gaseous phase, Boreskov (9) found formaldehyde to be the main product of this reaction; the formation of carbon monoxide was explained as a result of a consecutive reaction. Boreskov found neither carbon dioxide nor hydrogen in the gaseous product; the latter experimental fact was explained by the nonexistence of a dehydrogenation step in the catalytic oxidation of methanol over several oxides, including MoO<sub>3</sub>.

The composition of gaseous products of methanol oxidation (CH<sub>2</sub>O, CO, and H<sub>2</sub>O) is the same on molybdenum trioxide with oxygen in gaseous phase and on mixed Fe-Mo-O catalysts, the difference being in the rather low temperature of oxidation on Fe-Me-O catalysts.

## EXPERIMENTAL METHODS

The MoO<sub>3</sub> used was of analytical grade from Merck, its surface area being 2.6 m<sup>2</sup>

(by adsorption of Ar at 78°K, where for the area of Ar molecule 16.6 A² was taken). Methanol used was the same as in Ref. (6), formaldehyde was obtained by evaporating solid paraformaldehyde of analytical grade from Lachema, carbon monoxide was prepared by decomposition of magnesium oxalate with freezing of sideproducts.

One g of MoO<sub>3</sub> was heat-treated *in vacuo* ( $10^{-5}$  Torr) for 15 hr at  $400^{\circ}$ C. Then the sample was joined with a reservoir of 500 cm³ and the gaseous mixture (with a pressure about 0.5 Torr) was analyzed with a mass spectrometer MCH 1302 (USSR) directly linked to the reservoir with the sample. The changes of the composition of the gaseous mixture were followed continuously with time at constant temperature (generally  $320 \pm 2^{\circ}$ C); in case of no changes observed the temperature was elevated up to  $400^{\circ}$ C.

The amount of methanol or another gas used in one dose was chosen in such a way that the number of gaseous molecules was approximatively the same as the number of oxygen atoms in the surface layer of MoO<sub>3</sub> (i.e., about 10<sup>19</sup>). Therefore, we may suppose that the reaction proceeds—in a prevailing manner—in the surface of molybdenum trioxide. In order to show the differences in the behavior of the deeper layers of oxygen in solid MoO<sub>3</sub>, the proce-

dure was in some cases repeated after the evacuation of the sample.

#### RESULTS

The time-course of the methanol concentrations and of its oxidation products is plotted in Fig. 1a. After this experiment, MoO<sub>3</sub> was evacuated at the same temperature (320°C) for 1 hr and then was joined with another reservoir with methanol. The oxidation of this methanol sample is shown in Fig. 1b. A large difference in the character of concentration changes can be seen from these two plots. The rate of methanol oxidation does not substantially differ in both cases, being even a little larger in case b. The maximum of the formaldehyde concentration is, in case a, much higher and appears later than after the second dose of methanol (case b). The more complete oxidation (to CO and CO<sub>2</sub>) proceeds in case b from the beginning of the methanol

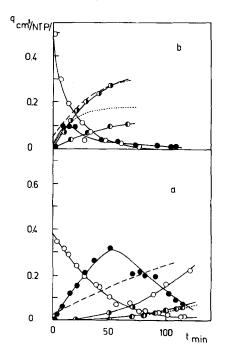


Fig. 1. The time-course of concentrations in the oxidation of methanol on molybdenum trioxide at 320°C: (a) the first dose of methanol; (b) the second dose of methanol after the evacuation of the sample. CH<sub>2</sub>OH (○); CH<sub>2</sub>O (●); CO (●); CO<sub>2</sub> (●); H<sub>2</sub>O (---); and H<sub>2</sub> (....).

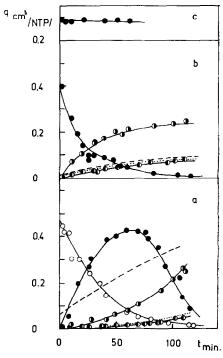


Fig. 2. The time-course of concentrations in the oxidation of formaldehyde and methanol at  $320^{\circ}$ C: (c) the first dose of formaldehyde; (a) the first dose of methanol; (b) the dose of formaldehyde after the evacuation of the sample. CH<sub>3</sub>OH ( $\bigcirc$ ); CH<sub>2</sub>O ( $\bigoplus$ ); CO ( $\bigoplus$ ); CO<sub>2</sub>( $\bigoplus$ ); H<sub>3</sub>O (---); and H<sub>2</sub> (...).

oxidation. Also the amount of liberated hydrogen in case b is much larger than in case a, where hydrogen started to appear after the maximum in formaldehyde concentration was attained.

With regard to these results it was interesting to follow the oxidation of formaldehyde on MoO3 in the same way as the oxidation of methanol. The results of formaldehyde oxidations on MoO3 are demonstrated in Fig. 2. In case c, formaldehyde was in contact with MoO<sub>3</sub> for 1 hr at 320° without any change in its composition; no oxidation proceeded when the temperature was elevated up to 400°C. Therefore, we have first oxidized methanol on another sample of MoO<sub>3</sub>—the typical course of this oxidation is shown in Fig. 2a; then this sample was evacuated for 1 hr at 320°C and was joined to a new reservoir filled with formaldchyde. The

time-course of formaldehyde concentration is plotted in Fig. 2b, its oxidation products being CO,  $CO_2$ ,  $H_2O$ , and  $H_2$ .

The oxidation of carbon monoxide was followed in the same way. It proceeds neither on a fresh sample of MoO<sub>3</sub>, nor on a sample previously reduced during the oxidation of methanol. The negative result with regard to the CO oxidation was the same when the temperature was elevated up to 400°C.

### Discussion

The results of the study of the interaction of CH<sub>3</sub>OH, HCHO, and CO with MoO<sub>3</sub> at 320°C—without oxygen in the gaseous phase—can be summarized as follows: (a) MoO<sub>3</sub> oxidized CH<sub>3</sub>OH to HCHO only under participation of a small part of its oxygen atoms, which is limited approximately to the surface oxygen. HCHO and CO were not oxidized on this unreduced MoO<sub>3</sub> at all. (b) A partly reduced MoO<sub>3</sub> was an agent for the deep oxidation of CH<sub>3</sub>OH and HCHO, the products of oxidation being mainly CO, H<sub>2</sub>, H<sub>2</sub>O, and partly CO<sub>2</sub>. CO was not oxidized at all.

The release of water into the gaseous phase is suggested to be proof for the participation of oxygen atoms from the solid phase in the oxidation reactions on MoO<sub>3</sub>; together with the prevailing selective function of this catalyst in presence of oxygen in gaseous phase, this fact might be explained as a function of some "redox" mechanism. For this reason it might be useful to correlate the reactivity of lattice oxygen and the catalytic activity of MoO<sub>3</sub> as oxidation catalyst according to the ideas published already on the strength of the lattice oxygen bond (10-13). Recently, a parallelism has been found in oxidation catalysis between the catalytic selectivity and the differential increase of the enthalpy of oxygen release from the catalyst with an increasing degree of its reduction (14). Those catalysts, where the removal of oxygen from the surface is easy, possess high activity for deep oxidation. On the contrary, those catalysts, where the removal of more oxygen atoms from the solid at the same site requires more energy, act as selective catalysts.

When we apply this idea to the behavior of molybdenum trioxide in methanol oxidation, we are obliged to suppose that the remaining oxygen atoms are more active than those from the surface. Such an effect, which is not thermodynamically probable (13), could be found out by the method of oxygen exchange between gaseous labeled oxygen and oxygen atoms of MoO<sub>3</sub>; this exchange, however, was measured by others (15) without similar effects. It is worth noting, that there are some other conditions between the experiments with the isotopic exchange of gaseous oxygen and the measurements of the oxygen pressure above the oxides, the main difference being in the substantially higher pressure of oxygen in the case of the exchange than that of the measurements of oxygen pressure. However, a simbatic relation for deep oxidation and an antibatic relation for selective oxidation has been found by Boreskov (13) between the catalytic activity on one side and the ability of oxygen exchange and oxygen release on the other side. Any direct relation among the degree of reduction of the oxide and the isotopic exchange has not been published; it seems, that the value of diffusion coefficient of lattice oxygen might be suitable for such a correlation.

The various functions of one oxidation catalyst in different oxidation reactions (deep, selective, or no catalytic action) cannot be explained only on the basis of differential increase of enthalpy of the oxygen removal from the catalyst too.

The idea about the prevailing role of the enthalpy of the release of lattice oxygen in deep and selective oxidation catalysis seems to be valid in the case when the oxidation of a substance A proceeds via the formation of surface complexes of the type, (a)

where A is in some manner bound to the

lattice oxygen O, Me being a cation of the oxide.

When A is bound to the surface via a complex (b) similar

the function of oxygen release might be overlapped by the bonding Me---A. The existence and the strength of the Me---A bonding would probably be a complicated function of the degree of the catalyst reduction, the type and the valency of Me cation playing an important role.

The existence of various species of chemisorption of substance A in "redox" reactions seems therefore to be an explanation for the selective and deep oxidation functions of the catalyst, which is more probable than that based on mobility only.

In our case—oxidation of methanol on MoO<sub>3</sub>—the existence of a complex of type (b) may be used for the explanation of experimental data: e.g., CH<sub>3</sub>OH might be bounded to Mo<sup>6+</sup> by e.g., an alcoholate bonding:

which decomposes under formation of formaldehyde and water, one H atom from the methanol molecule being bond to a surface oxygen. On molybdenum of lower valency—probably Mo<sup>4+</sup>—methanol and formaldehyde are decarbonylized and CO with H<sub>2</sub> appears in gaseous phase. Only a small part of bound

could for sterical reasons be oxidized to  $CO_2$ , the oxidation of H to  $H_2O$  being also sterically hindered.

Our results do not seem to be in agreement with the conclusions of Boreskov's paper: the formation of CO in methanol oxidation on MoO<sub>3</sub> is probably not a simple consecutive reaction, but is caused by the reduction of the MoO<sub>3</sub> surface (see a, b on Fig. 1). The absence of  $H_2$  molecules in the gaseous phase is not necessarily the evidence for the nonexistence of the dehydrogenation step in oxidation; hydrogen atoms of methanol are probably bound with oxygen from the MoO<sub>3</sub> surface in case it has not yet been reduced. This phenomenon cannot be observed by measuring the oxidation of methanol in presence of oxygen in gaseous phase. In this case the oxidation probably proceeds only in the surface layer of MoO<sub>3</sub> which is immediately resaturated with oxygen.

It can be concluded that the selective oxidation of methanol on MoO<sub>3</sub> is joined with its unreduced surface. The function of the Fe<sup>3+</sup> cation in mixed Fe-Mo-O catalyst may help (together with other functions) to maintain the higher value of molybdenum valency.

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